

Application Note AN-PAN-1005

Online analysis of calcium and magnesium in brine

Chlorine is produced from salt (brine) via three major technologies. In Europe, the membrane technology now accounts for 85% [1], followed by the diaphragm process (10%), while the mercury cell process has been completely phased out (since 2020). Other minor technologies account for the remaining 5% of chlor-alkali production.

When producing chlorine through the membrane electrolysis process, the purity of the brine is very important. The presence of impurities such as calcium and magnesium can shorten the performance and lifetime of the membranes or can damage the electrodes. Partial membrane blockage leads to higher electrical operational costs and the high cost associated with replacing membranes.

This Process Application Note focuses on monitoring calcium and magnesium impurities (known as hardness) in brines used for the production of chlorine and caustic soda during the chlor-alkali process. By utilizing online process analysis, important information about the impurity removal process can be obtained in a timely manner, and costly membrane blockages can be avoided.



INTRODUCTION

Chlorine and caustic soda are used as feedstock materials in production processes for several markets (e.g., pulp and paper, petrochemical, and pharmaceutical). The chlor-alkali process produces chlorine and caustic soda via the electrolysis of sodium chloride solutions (i.e. brine) (**Reaction 1**). This process is responsible for 95% of chlorine produced globally [**2**]. Hydrogen (H_2) is a co-product of the chlor-alkali process,

and can be used to produce other chemicals (e.g., HCl, NH_3 , H_2O_2 , CH_3OH , and more) or even as a utility to produce steam and electricity.

The most commonly applied electrolysis technique in Europe is the **membrane cell technique** (85%) [1]. All new plants are based on membrane cell electrolysis of brine, which does not include mercury and asbestos like the other two major technologies.

$2NaCl + 2H_2O \rightarrow 2NaOH + H_2 + Cl_2$

Reaction 1. Overall reaction of the chlor-alkali process.



Figure 1. Diagram of membrane cell technique for the production of chlorine. Adapted from www.eurochlor.org.

Brine purification is an unavoidable step to preserve the expensive membranes and prolong the efficiency of the electrolysis process. The level of impurities including calcium (Ca^{2+}) and magnesium (Mg^{2+}) (otherwise known as hardness) is reduced in two treatment steps.



After primary treatment with sodium hydroxide and sodium carbonate, the precipitated impurities $(CaCO_3, Mg(OH)_2)$ are filtered or settled out and the purified brine passes through an ion exchange unit (secondary treatment) prior to the electrolysis process (Figure 1). The efficiency of the settling and resin treatments can be calculated based on accurate determination of hardness before and after the secondary treatment commences.



Figure 2. Simplified illustration of a chlor-alkali plant with stars noting where online process analyzers can be integrated.

After the brine goes through a secondary treatment with an ion exchange resin, impurity concentrations can be reduced by a factor of 1000. Upstream control of brine quality helps to overcome costly problems, such as the blockage of electrolysis membranes or shutdown due to premature exhaustion of the ion exchange resin. Thus, hardness determination in ultrapure brine is necessary to prevent damage downstream in the electrolysis process. Very costly remediation procedures are necessary if the membranes are

fouled.

Traditionally, the brine can be analyzed by laboratory titration (or photometry). However, this methodology does not provide timely results and requires human intervention to implement the laboratory analysis results to the process. Online process analysis allows constant monitoring of brine quality without long waiting times in the laboratory, giving more accurate and representative results directly to the control room.

APPLICATION

The brine quality must be constantly monitored to avoid blockage of electrolysis membranes or shutdown due to premature exhaustion of the ion exchange resin. Metrohm Process Analyzers can be used in several stages of the process (**Figure 2**), from high feed concentrations of hardness to very low concentrations in the ultrapure brine. Upstream control of total hardness quality before the secondary treatment ion exchange is commonly measured during an EDTA titration, with the inflection point determined via dipping probe with color indicator (**Figure 3**). The trace amount of hardness present after the secondary purification process is commonly determined photometrically with a color indicator (**Figure 4**).





Figure 3. Online titration for total hardness in brine (mg/L range) at the inlet of the resin treatment. Data provided by the Metrohm Process Analytics 2035 Process Analyzer.



Figure 4. Initial (red) and final (blue) online colorimetric measurements of hardness in brine (µg/L range). Data provided by the Metrohm Process Analytics 2035 Process Analyzer.



Online analysis is a dependable solution, offering both extremely low detection limits and highly accurate results, giving extra assurance that expensive company assets are being safeguarded. Process analyzers from Metrohm Process Analytics will monitor the total hardness concentration in brine around the clock and send out automatic alerts if there is a breakthrough of impurities from the ion exchanger, allowing quick action to be taken before the membranes are affected.



Figure 5. Metrohm Process Analytics offers the 2060 Process Analyzer (left) and the 2035 Process Analyzer (right) for continuous online brine monitoring in chloralkali plants

REMARKS

Other applications are available for the chloralkali industry like: acidity, carbonate, hydroxide, silica, alumina, ammonia, iodate, strontium, barium, and chlorine.

Table 1. Ranges and detection limits of hardness in brine before and after the secondary purification (ion exchange resin) treatment.

| Analyte | Concentration range | Detection limit |
|------------------------|---------------------|-----------------|
| Inlet resin treatment | | |
| Ca ²⁺ | 0–20 mg/L | 0.05 mg/L |
| Mg ²⁺ | 0–10 mg/L | 0.18 mg/L |
| Outlet resin treatment | | |
| Ca ²⁺ | 0-20 μg/L | 0.4 μg/L |
| Mg ²⁺ | 0-20 μg/L | 0.4 μg/L |

FURTHER READING Related documents

<u>White Paper: Optimizing chlor-alkali production</u> <u>through online chemical analysis</u> <u>Brochure: Chlor-Alkali Industry – Dependable</u> online, inline, and atline solutions for your process needs



Related applications for the chlor-alkali industry

Analysis of ammonia with the manufacture of ammonia-saturated brine in the Solvay process Online determination of lithium in brine streams with ion chromatography Online Determination of Anions in 50% NaOH and 50% KOH by IC (ASTM E1787-16)

BENEFITS FOR ONLINE ANALYSIS

- Safer working environment and automated sampling
- Increase membrane lifetime by better and faster process control
- Increased final product quality (NaOH) due to online monitoring of ion exchanger efficiency
- Fully automated diagnostics automatic alarms for when brine streams are out of set specification parameters



REFERENCES

- 1. How Are Chlorine and Caustic Soda Made? Euro Chlor 17.
- 2. Euro Chlor. Chlor-Alkali Industry Review; Technical report; Euro Chlor 17, 2019.

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CONFIGURATION





2035 Process Analyzer Photometric

用于光度分析的 2035 Process Analyzer 程分析,包 括一个在大度范内均可十分定的型光度模,且可通其拌 功能保持恒温。可提供款型的分析:比色皿系或光浸探 。比色皿系小巧,可降低消耗,但能提供光路以保高敏 度。光浸探著地展了我的用范,通使用内部品稀步使高 度品的精量更加方便,且具有短于比色皿系的光路。 光度分析是一广泛使用的常技,可以在用水甚至和的水 溶液中定子成如、和。不利的品基特性如品色或度等 可通差分量去除,量前后加入色。

2060 Process Analyzer

2060 Process Analyzer 是一在湿化学分析,用于无数 用。此程分析提供了一个新的模化概念,由一个称《主 机》的中心平台成。

主机由部分成。上部包含触摸屏和工算机。下部含有 柔性取部,其中放有用于分析的硬件。如果主取部容量 不足以分析挑,那主机可以展多四个外的取部机,以保 有足的空来最具挑性的用。附加机的配置方式使每个 取部机可以与具有集成(非接触式)液位的合使用,以增 加分析的正常行。

2060 Process Analyzer 提供不同的湿化学技:滴定法、舍滴定法、光度定、直接量和准添加入法。

足所有目要求(或足的所有需求),可提供品理系,以保分 析解决方案可靠。我可以提供任何品理系,如冷却或加 、和脱气、等。

