Application Note AN-EC-014

Oxygen Reduction Reaction with the Rotating Ring Disk Electrode

The oxygen reduction reaction (ORR) is one of the most studied reactions in the field of electrocatalysis. The ORR in aqueous acidic electrolyte can proceed through different pathways depending on the reaction conditions. In most cases, the desired reaction is the 4-electron process shown in Equation 1. Other possible reaction pathways include the combinations of Equations 2 and 3, where H_2O_2 is formed as an intermediate, and Equations 2 and 4, where the reduction is incomplete.

$$O_2 + 4H + + 4e^- \rightarrow 2H_2O \quad (1)$$

$$O_2 + 2H^+ + 2e^- \rightarrow H_2O_2 \quad (2)$$

$$H_2O_2 + 2H^+ + 2e^- \rightarrow 2H_2O \quad (3)$$

$$2H_2O_2 \rightarrow 2H_2O + O_2 \quad (4)$$

If hydrogen peroxide (H_2O_2) is formed as a product or intermediate during the ORR, it can be detected electrochemically through its oxidation reaction, Equation 5.

$$H_2O_2 \rightarrow O_2 + 2H^+ + 2e^- \quad (5)$$

The ORR is generally studied in hydrodynamic conditions using a rotating working electrode (WE) to induce forced convection within the electrochemical cell. This strategy is applied to achieve a stable mass transfer limited current density that may otherwise be difficult to maintain because of the slow kinetics of the reaction. In this application note, a rotating ring disk electrode (RRDE) set up is used to study the ORR.

EXPERIMENTAL CONDITIONS

An Autolab PGSTAT302N potentiostat/galvanostat fitted with the BA module, a dual-mode bipotentiostat, was used in combination with the Autolab RRDE hardware. The measurements were carried out in a four electrode configuration using the Autolab RRDE electrochemical cell.

Since the electrochemical signals from Pt electrodes are sensitive to system impurities, all cell components in contact with the electrolyte were thoroughly cleaned. The cleaning procedure consists of soaking the components a diluted solution of H_2SO_4 with H_2O_2, followed by rinsing several times with boiling water. The working electrodes were the Pt disk (WE1) and Pt ring (WE2), which are both built into a single RRDE tip. The RRDE tips have a theoretical collection efficiency of 24.9% based on the geometry of the disk and the ring. Determination of the experimental collection efficiency and the meaning of the theoretical collection efficiency value are outside the scope of this application note. The counter electrode (CE) was a platinum sheet and the reference electrode (RE) was a double junction Ag/AgCl electrode with 3 M aqueous KCl solution in the inner compartment and the working electrolyte (0.5 M H_2SO_4) in the outer compartment. Both the CE and the RE were inserted into the cell at a height slightly above that of the bottom of the RRDE electrode tip in order to avoid disturbing the hydrodynamic flow profile. The 0.5 M H_2SO_4 electrolyte was purged with high purity O_2 gas for fifteen minutes prior to beginning the experiments in order to reach a saturated concentration of dissolved O_2. During the measurement, a blanket of O_2 gas was maintained over the surface of the electrolyte to ensure that the concentration of dissolved O_2 remained stable.

The experimental procedure *hydrodynamic linear sweep with RRDE* was applied using the NOVA software. At the disk, linear voltammetry staircase sweeps from 0.70 to –0.20 V vs. Ag/AgCl were applied with various electrode rotation rates (ω). At the ring, the potential was fixed at 1.00 V and the current response was recorded.

EXPERIMENTAL RESULTS

Figure 1 shows the results of a typical ORR RRDE experiment. The blue curves correspond to the current at the Pt disk (WE1) as the *E* is swept from 0.70 to –0.20 V at a scan rate of 50 mV s^{-1} with various electrode rotation rates (ω). The red curves correspond to the current signal at the Pt ring (WE2), whose potential is fixed at a value of 1.00 V, at the same ω values as the disk.

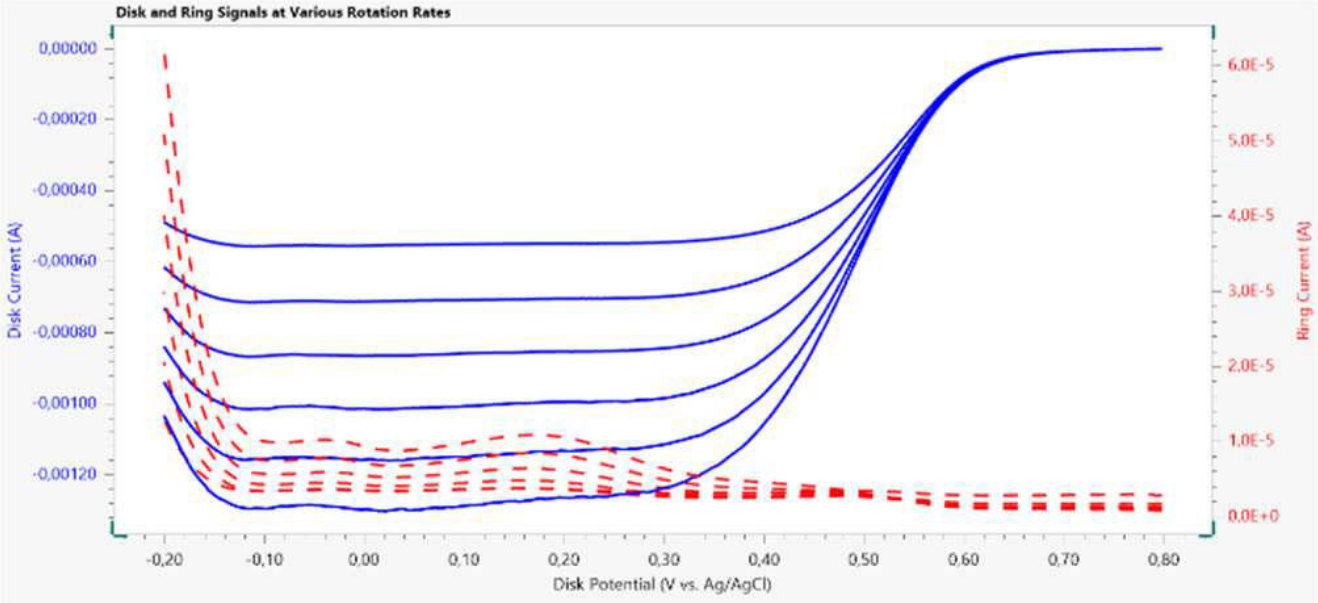

Figure 1. Plot of the disk (blue solid lines) and ring (red dashed lines) current data vs. the disk potential, collected during the hydrodynamic RRDE study of the ORR using a Pt disk and Pt ring.

The ω values varied between 500 and 3000 RPM; they were chosen with a square root relationship for intuitive representation on the Levich plot. As the potential at the disk is swept from high to low values, the onset of ORR gives rise to a negative (cathodic) signals that is observable at approximately 0.65 V.

The current increases with decreasing potential then reaches a plateau region at approximately E = 0.20 V to –0.10 V. This plateau is also known as the mass transfer limited region of the voltammetry profile where the rate of the ORR reaction is limited by the availability of oxygen at the electrode surface. The cathodic current increases in magnitude with increasing ω according to the Levich relationship. At the lowest potential values (i.e., lower than –0.10 V), cathodic current decreases in magnitude as the adsorption of hydrogen on the Pt electrode surface interferes with the ORR. The potential at the ring is fixed at 1.00 V, thus the X-axis of the graph in Figure 1 does not apply to the ring data. Although the potential of the ring is fixed, the current signal at the ring changes as the potential of the disk is swept. This is because the disk and the ring are in close proximity of each other (there is a separation of 375 µm between the disk and ring). Thus, the chemical environment at the disk influences the ring. As oxygen is reduced at the disk, reaction products, such as H_2O_2, diffuse from the disk to the ring and may undergo further reaction. The oxidation of H_2O_2 gives rise to a positive (anodic) current signal and therefore the current at the ring is indicative of H_2O_2 production at the disk. The anodic current at the ring increases as the potential of the disk is swept to low values that give rise to ORR at a significant rate. When the disk current is limited by mass transfer (plateau region of the blue curves), the current corresponding to H_2O_2 oxidation at the ring continues at a relatively stable value. When the cathodic disk current decreases due to the presence of adsorbed hydrogen on its surface, the ring current increases sharply; this indicates a change in the ORR mechanism where a greater proportion of the reaction is now following a pathway that favors H_2O_2 production.

Figure 2 shows the Levich and Koutecký-Levich plots

for the ORR which demonstrate the relationship between the current and the rotation rate at a fixed potential.

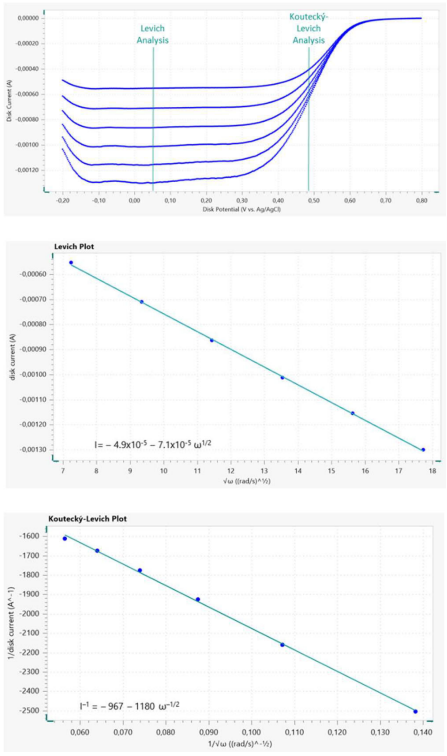

Figure 2. Linear sweep voltammetry profiles (top) from the disk electrode at various rotation rates; the potential value for the Levich and Koutecký-Levich analyses are indicated. Levich (middle) and Koutecký-Levich (bottom) plots.

When the potential value is selected within the mass-transfer limiting plateau of i vs. E curves, the Levich plot follows a linear relationship according to Equation 6.

$$i_l = 0.62 \times AnFD^{2/3}v^{-1/6}C\sqrt{\omega} \qquad 6$$

When the potential is selected from the region where the current is under a mixture of kinetic and mass transfer control, the Koutecky-Levich plot is liner according to Equation 7.

$$\frac{1}{i} = \frac{1}{i_k} + \frac{1}{0.62 \times AnFD^{2/3}v^{-1/6}C\sqrt{\omega}} \qquad 7$$

For both Equations 6 and 7, the variables are defined as:
A (cm^2) is the geometric area of the disk F (= *96485 C* mol^{-1}) is the Faraday's constant D ($cm^2 s^{-1}$) is the diffusion coefficient of O_2 in the electrolyte v ($cm^2 s^{-1}$) is the kinematic viscosity of the electrolyte C ($mol\ cm^{-3}$) is the concentration of O_2 in the electrolyte ω ($rad\ s^{-1}$) is the angular frequency of rotation n is the number of electrons involved in the reaction

The Levich and the Koutecky-Levich plots can be fitted using linear regression to calculate the slopes and intercepts. For the Koutecky-Levich plot, the kinetic current i_k is calculated from the y-intercept which is equal to $1/i_k$. According to Equation 8, the i_k value can be related to the rate constant for electron transfer k. In order for Equation 8 to be applied, the number of electrons involved in the reaction n must be known.

$$i_k = nFAkC \qquad 8$$

Information about the dominant mechanistic pathway at a given potential value can be elucidated based on the presence of H_2O_2 detected at the ring (WE2). The data presented in Figure 1 indicates that ORR proceeds via a mixture of the four-electron and two-electron pathways at potential values within the mass transfer limited plateau. At potential values less than –0.10 V the two-electron mechanism becomes dominant, as evidenced by the increase in H_2O_2 detected at the ring.
It is possible to calculate the diffusion coefficient of oxygen in the system using the slope value from the linear regression applied to the Levich plot in Figure 2. The variables relating to the system that are required for this calculation are listed in Table 1. The concentration of O_2 in the electrolyte is assumed to be equal to its solubility; in other words the solution is saturated. This experiment yields a diffusion coefficient value for oxygen in the electrolyte of $7.6E{-}5\ cm^2\ s^{-1}$ when assuming a four-electron process and $2.2E{-}5\ cm^{-2}\ s^{-1}$ when assuming two electrons are transferred. In reality, both processes contribute to the measured electrochemical signal. The diffusion coefficient value is high when compared with a literature value of $1.4E{-}5\ cm^2\ s^{-1}$ (see references). This property is sensitive to experimental parameters such as the concentration of O_2 in the electrolyte, which is likely to be the most significant source of uncertainty in this measurement.

Table 1. System variables for the oxygen reduction reaction in 0.5 M H2SO4 electrolyte at room temperature.

Parameter	Value	Unit
Kinematic viscosity	0.010	$cm^2\ s^{-1}$
Solubility of O_2	1.1E-6	$mol\ cm^{-3}$
Electrode geometric area	0.20	cm^2

CONCLUSIONS

In this application note, the Autolab RRDE system was used to study the oxygen reduction reaction with a Pt disk/Pt ring electrode. The H_2O_2 formed at the disk electrode during ORR was detected at the ring electrode; its presence was used as an indicator of the reaction pathway. The Levich and Koutecky-Levich plots were fitted using linear regression. The resulting equations can be used to calculate the diffusion coefficient O_2 in the electrolyte, the number of electrons transferred during the reaction, and the rate constant for electron transfer.

REFERENCES

1. N.A. Anastasijevic et al. J. Electroanal. Chem. 229 (1987) 305
2. Nenad M. Markovic et al. J. Phys Chem. 99 (1995) 3411
3. Carlos M. Sanchez–Sanchez and Allen J. Bard. Anal. Chem. 81 (2009) 8094
4. Francisco J. Vidal-Iglesias et al. Electrochem. Commun. 15 (2012) 42.
5. Alfred B. Anderson. Electrocatal. 3 (2012) 176.
6. K–L. Hsueh et al. Electrochimica Acta. 28 (1983) 691.

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CONFIGURATION



Autolab PGSTAT204

The PGSTAT204 combines the small footprint with a modular design. The instrument includes a base potentiostat/galvanostat with a compliance voltage of 20 V and a maximum current of 400 mA or 10 A in combination with the BOOSTER10A. The potentiostat can be expanded at any time with one additional module, for example the FRA32M electrochemical impedance spectroscopy (EIS) module.

The PGSTAT204 is an affordable instrument which can be located anywhere in the lab. Analog and digital inputs/outputs are available to control Autolab accessories and external devices are available. The PGSTAT204 includes a built-in analog integrator. In combination with the powerful NOVA software it can be used for most of the standard electrochemical techniques.



Autolab PGSTAT302N

This high end, high current potentiostat/galvanostat, with a compliance voltage of 30 V and a bandwidth of 1 MHz, combined with our FRA32M module, is specially designed for electrochemical impedance spectroscopy.

The PGSTAT302N is the successor of the popular PGSTAT30. The maximum current is 2 A, the current range can be extended to 20 A with the BOOSTER20A, the current resolution is 30 fA at a current range of 10 nA.



Autolab Electrocatalysis RRDE cell

The Autolab RRDE cell is a complete electrochemical cell designed for experiments under forced convection with the Autolab RRDE (or Autolab RDE2). The kit consists of a glass vessel with a volume of 300 mL, fitted with a thermostatic jacket for temperature control.

All the parts that can come in contact with the solution can be cleaned in aggressive conditions, making the cell suitable for typical electrocatalysis experiments or sensitive interfacial electrochemistry measurements.



Rotating Ring Disk Electrode

The Autolab RRDE is a low-noise rotating ring disk electrode that can be used to perform electrochemical measurements under controlled hydrodynamic conditions. The ring and disk electrode assembly provides the means to detect reaction intermediates in situ through collection experiments.
The Autolab RRDE uses 2 identical friction-less mercury contacts for low noise measurements and can be used with any Autolab potentiostat/galvanostat fitted with the BA, dual-mode bipotentiostat module.
The rotation speed of the RRDE is controlled manually with the button on the front of the motor control unit. The RRDE can also be controlled remotely with the Autolab software. The rotation speed can be varied continuously between 100 and 10,000 rpm with a resolution of 1 rpm.

Advanced software for electrochemical research

NOVA is the package designed to control all the Autolab instruments with USB interface.

Designed by electrochemists for electrochemists and integrating over two decades of user experience and the latest .NET software technology, NOVA brings more power and more flexibility to your Autolab potentiostat/galvanostat.

NOVA offers the following unique features:

- Powerful and flexible procedure editor
- Clear overview of relevant real-time data
- Powerful data analysis and plotting tools
- Integrated control for external devices like Metrohm Liquid Handling devices

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